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10/088912-13-06173
JC13 Rec'd PCT/PTO 25 MAR 2002

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DESCRIPTION

AROMATIC MONOVINYL RESIN COMPOSITION

Technical Field

The present invention relates to an aromatic monovinyl resin composition less in residual amount of aromatic monovinyl monomers and a method for producing the same, and, more particularly, to an aromatic monovinyl resin composition excellent in heat stability at molding and suitable for use as materials directly contacting with foods, etc. Furthermore, the present invention relates to a product comprising an aromatic monovinyl resin composition and having good color tone and appearance and developing less odor.

Background Art

Because of their excellent moldability, aromatic monovinyl resins are widely used as materials for electric articles, various industrial materials, materials of miscellaneous goods and containers for foods, packaging materials, etc.

However, as to aromatic vinyl resins, for example, polystyrenes, the resulting products sometimes suffer from the problem of development of odor if amounts of styrene monomers contained in the resins are large. Furthermore, if dimers or trimers of styrene monomers are contained in large amounts in the resins,

they cause unfavorable phenomena such as deterioration of heat resistance, and volatilization and retention of them in the mold at injection molding, which are transferred to the resulting molded products or they
 5 cause problems such as reduction of productivity due to increase in the number of cleaning of the mold.

As for the odor of products, JP-A-7-149817 and JP-A-7-149818 propose to reduce the odor with use of phenolic heat deterioration inhibitors, but this
 10 technique has a defect of inferior color tone of the resulting products. Moreover, for inhibiting the production of dimers and trimers, JP-5-170825 proposes to add phenolic heat deterioration inhibitors at
 15 polymerization step or devolatilization step in production of resin, but this method also has the defect of inferior color tone of the resulting products as above.

On the other hand, U.S. Patent Nos. 4325863, 4338244 and 5175312 propose to stabilize polymers with
 20 addition of 3-arylbenzofuranone, but they make no mention of relation between concentration of the aromatic monovinyl monomer and color tone of the resulting products.

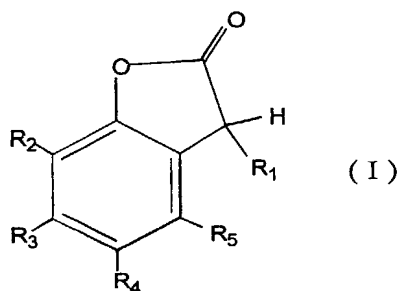
Furthermore, if the resins contain large
 25 amounts of the aromatic monovinyl monomer, or dimers and trimers thereof, the following problems may be caused in production of non-foamed sheets and foamed sheets.

That is, if the monomer is present in a large amount in production of non-foamed sheets (molding), removal of gas from dice is not smoothly carried out and the gas is locally present, which sometimes causes formation of die lines on the surface of sheets (a phenomenon of occurrence of lines on the surface of the sheets). If the dimer and the trimer are present in large amounts, they condense and stay at the dice part, and are deposited on the surface of the sheet to form contaminants. These phenomena sometimes bring about serious problems such as bad appearance of the products obtained after forming and unsatisfactory printing on the products.

Moreover, if amount of the monomer is large in production of foamed sheets (molding), the monomer is condensed in the mandrel of extruder, especially, in a mass production machine, and the condensed liquid deposits on the surface of the foamed sheet (sagging phenomenon) to cause serious problems such as bad appearance of the products obtained after forming and unsatisfactory printing on the products. Furthermore, if amounts of the dimer and the trimer are large, extension viscosity of the resin lowers, sometimes resulting in narrow molding width due to drawdown at the time of forming and reduction of productivity.

In order to solve these problems, it is desired that amounts of residual low molecular components such as styrene monomer and dimer and trimer

700,000 and (b) a 3-arylbenzofuranone represented by the following formula (I):



(in the formula, R_1 represents a substituted or unsubstituted carbocyclic aromatic group or a substituted or unsubstituted heterocyclic aromatic group and R_2 , R_3 , R_4 and R_5 represent independently a hydrogen atom or an alkyl group of 1-5 carbon atoms), wherein amount of the 3-arylbenzofuranone is 0.006-0.5% by weight based on the weight of the polymer and residual amount of the aromatic monovinyl monomer remaining in the aromatic monovinyl resin composition is not more than 100 ppm.

Furthermore, the present invention relates to a foamed sheet comprising said aromatic monovinyl resin composition and a formed product obtained therefrom.

Moreover, the present invention relates to a non-foamed sheet comprising said aromatic monovinyl resin composition and a formed product obtained therefrom.

Brief Description of Drawing

FIG. 1 shows a formed product obtained from a foamed sheet.

5 Best Mode for Carrying Out the Invention

The present invention will be explained in detail below.

As mentioned above, the present invention is an aromatic monovinyl resin composition comprising (a)
10 a polymer comprising an aromatic monovinyl monomer and having a weight average molecular weight of 150,000-700,000 and (b) a 3-arylbenzofuranone represented by the above formula (I), wherein amount of the 3-arylbenzofuranone is 0.006-0.5% by weight based on the
15 weight of the polymer and residual amount of the aromatic monovinyl monomer remaining in the aromatic monovinyl resin composition is not more than 100 ppm.

As the aromatic monovinyl monomer used as a starting material for obtaining the polymer (a)
20 comprising an aromatic monovinyl monomer, mention may be made of not only styrene alone, but also mixtures of styrene with other vinyl monomers copolymerizable with styrene. Here, examples of the other vinyl monomers copolymerizable with styrene are methyl methacrylate,
25 methyl acrylate, butyl acrylate, ethyl methacrylate, halogen-containing vinyl monomers, α -methylstyrene, o-methylstyrene, m-methylstyrene, p-methylstyrene, etc., and one or more of them can be used. These vinyl

monomers copolymerizable with styrene can be used in a proportion of generally not more than 60% by weight, preferably not more than 50% by weight based on all the monomers.

5 Moreover, the aromatic monovinyl polymers may contain rubber components such as polybutadiene, SBR, polyisoprene, nitrile rubber, natural rubbers, etc.

 In the present invention, as a heat deterioration inhibitor, there is used one which has a structure capable of effectively trapping radicals generated in the absence of oxygen to perform stabilization, namely, a 3-arylbenzofuranone represented by the above formula (I). Amount of the heat deterioration inhibitor is 0.006-0.5% by weight, preferably 0.008-0.3% by weight, more preferably 0.01-0.2% by weight based on the weight of the polymer. If the amount of the 3-arylbenzofuranone is less than 0.006% by weight, the effect to inhibit the production of the aromatic monovinyl monomer and dimer or trimer thereof at the devolatilizing step is insufficient, and products less in the contents of them cannot be obtained. Moreover, if the amount is less than 0.006% by weight, the effect to inhibit the production of styrene monomer due to the heat decomposition of the polymer at molding is insufficient, and since it becomes very difficult to keep amount of the residual styrene monomer in the products at low level, products of satisfactory color tone cannot be obtained. This is

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5 Examples of the heat deterioration inhibitors
are 5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-
benzofuran-2-one, 5,7-di-tert-butyl-3-(2,5-
dimethylphenyl)-3H-benzofuran-2-one, 5,7-di-tert-butyl-
3-(3,4-dimethylphenyl)-3H-benzofuran-2-one, etc. Among
0 them, preferred is 5,7-di-tert-butyl-3-(3,4-
dimethylphenyl)-3H-benzofuran-2-one.

In the present invention, the residual amount of the aromatic monovinyl monomer is not more than 100 ppm, preferably not more than 95 ppm. When a rectangular parallelepiped container of 95 mm in opening width, 55 mm in length, 96 mm in depth and 2 mm in thickness is prepared from polystyrene and impact-resistant polystyrene by injection molding, 200 ml of warm water of 90°C is charged in this container, and after lapse of 3 minutes, odor of this warm water is examined, the problem of odor is markedly improved and color tone of the product is also markedly improved in the case of the residual amount of the aromatic monovinyl monomer being not more than 100 ppm. On the other hand, in the case of the residual amount of the aromatic monovinyl monomer being more than 100 ppm, color tone of the product is inferior even if said 3-arylbenzofuranone is added in the desired amount, and

The aromatic monovinyl resin composition obtained by the method of the present invention may contain usual additives, such as lubricants, antioxidants, ultraviolet absorbers, releasing agents, plasticizers, dyes, pigments, various fillers, etc., if
5 required. Furthermore, there may also be added other polymers such as general polystyrenes, styrene-butadiene copolymer elastomers, partially or completely hydrogenated styrene-butadiene copolymer elastomers,
10 polyphenylene ethers, etc.

The aromatic monovinyl resin composition of the present invention can be made into a foamed sheet, and this foamed sheet can be made into a formed product. In production of a foamed sheet using the
15 aromatic monovinyl resin composition of the present invention, the influence, on the product, of the aromatic monovinyl monomer condensed in the mandrel of extruder is investigated to find that poor appearance and inferior printability are not caused, and
20 appearance of the product is markedly improved and color tone of the product is also superior when the residual amount of the aromatic monovinyl monomer is not more than 100 ppm. On the other hand, when the amount exceeds 100 ppm, poor appearance and inferior
25 printability are seen.

Moreover, when the total amount of the residual dimer and trimer of the aromatic monovinyl monomer is not more than 0.4% by weight, the product

has little unevenness in thickness, and appearance of the foamed sheet and the formed product obtained from the sheet is also improved. The surface of the formed product is observed under magnification by a light
5 microscope to find that cell collapse hardly occurs and the surface is smooth.

The aromatic monovinyl resin composition of the present invention can also be made into a non-foamed sheet, and this non-foamed sheet can be made
10 into a formed product. As above, die lines are not formed in production of the non-foamed sheet, and appearance of the product is markedly improved when the residual amount of the aromatic monovinyl monomer is not more than 100 ppm. Further, color tone of the
15 product is also good.

When the total amount of the dimer and trimer of the aromatic monovinyl monomer is not more than 0.4% by weight, deposition of foreign matters is visually examined to find no deposition of the foreign matters,
20 and appearance of the product is markedly improved. On the other hand, if the amount exceeds 0.4% by weight, the foreign matters deposited on the dice part are transferred to the sheet to damage the appearance of the product.

25 Next, the method for producing the aromatic monovinyl resin composition of the present invention will be explained.

Aromatic monovinyl polymers, for example,

polystyrene produced in industrial scale is mostly produced by radical polymerization, and, in this case, styrene monomers and dimers or trimers thereof are produced much in devolatilization of unreacted materials and/or solvent at the devolatilizing step or due to the heat decomposition of the polymer just after devolatilization, and the resulting products contain them in large amounts. Furthermore, when molded products are obtained using these resins by injection molding, blow molding, extrusion molding, etc., amounts of the styrene monomer, and dimers and trimers thereof further increase owing to the thermal history at molding.

Amount of the monomer remaining in industrially produced polystyrene is about 200-400 ppm, and it is very difficult to obtain a polystyrene containing the monomer in an amount of, for instance, not more than 100 ppm. Hitherto, in many cases, polystyrene is obtained by polymerization with heat initiation radicals and/or polymerization initiator radicals produced by the reaction of styrene monomer. In this case, amounts of the dimer and trimer of the styrene monomer can be reduced by increasing the proportion of the polymerization initiator radicals, but they are again produced due to the heat decomposition at the devolatilizing step, and thus there is the limit in reduction of the amounts of the dimer and the trimer.

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octane, 1,1-bis(t-butylperoxy)-3,3,5-trimethyl-
cyclohexane, 1,1-bis(t-butylperoxy)cyclohexane, n-
butyl-4,4-bis(t-butylperoxy)valerate, etc., dialkyl
peroxides such as di-t-butyl peroxide, t-butylcumyl
5 peroxide, dicumyl peroxide, α,α' -bis(t-
butylperoxyisopropyl)benzene, 2,5-dimethyl-2,5-di(t-
butylperoxy)hexane, 2,5-dimethyl-2,5-di(t-
butylperoxy)hexyne-3, etc., diacyl peroxides such as
acetyl peroxide, isobutyryl peroxide, octanoyl
10 peroxide, decanoyl peroxide, lauroyl peroxide, 3,5,5-
trimethylhexanoyl peroxide, benzoyl peroxide, 2,4-
dichlorobenzoyl peroxide, m-toluoyl peroxide, etc.,
peroxydicarbonates such as diisopropyl
peroxydicarbonate, di-2-ethylhexyl peroxydicarbonate,
15 di-n-propyl peroxydicarbonate, dimyristyl
peroxydicarbonate, di-n-ethoxyethyl peroxydicarbonate,
dimethoxyisopropyl peroxydicarbonate, di-(3-methyl-3-
methoxybutyl) peroxydicarbonate, etc., peroxy esters
such as t-butyl peroxyacetate, t-butyl
20 peroxyisobutyrate, t-butyl peroxy-pivalate, t-butyl
peroxyneodecanoate, cumyl peroxyneodecanoate, t-butyl
peroxy-2-ethylhexanoate, t-butyl peroxy-3,3,5-
trimethylhexanoate, t-butyl peroxy-laurate, t-butyl
peroxybenzoate, di-t-butyl diperoxyisophthlate, 2,5-
25 dimethyl-2,5-di(benzoylperoxy)hexane, t-butylperoxy
isopropyl carbonate, etc., ketone peroxides such as
acetylacetone peroxide, methyl ethyl ketone peroxide,
cyclohexanone peroxide, 3,3,5-trimethylcyclohexanone

peroxide, methylcyclohexanone peroxide, etc., hydroperoxides such as t-butyl hydroperoxide, cumene hydroperoxide, diisopropylperbenzene hydroperoxide, p-menthane hydroperoxide, 2,5-dimethylhexane-2,5-dihydroperoxide, 1,1,3,3-tetramethylbutyl hydroperoxide, etc., and the like.

Furthermore, there may also be used 2,2'-azobisisobutyronitrile, 2,2'-azobis(2-methylbutyronitrile), 1,1'-azobis(1-cyclohexanecarbonitrile), etc. which are azo initiators.

These organic peroxides or azo initiators may be used each alone or in combination of two or more.

As for the polymerization conditions, bulk
15 polymerization may be carried out with starting the
polymerization at 20-180°C depending on the
decomposition temperature of the organic peroxides used
as the polymerization initiators. To this bulk
polymerization system can be optionally added chain
20 transfer agents, solvents, heat stabilizers such as
general antioxidants, mineral oils, silicone oils, etc.

Examples of the chain transfer agents are α -methylstyrene linear dimers, mercaptanes, terpenes and halogen compounds such as n-dodecyl mercaptan, t-dodecyl mercaptan, 1-phenyl-2-fluorene, dipentene, 25 chloroform, etc., turpentine such as turpenolene, etc., and the like. Amount of the chain transfer agents used has no special limitation, and generally it

is about 0.005-0.1% by weight based on the monomers.

Examples of the solvents which are optionally used are aromatic hydrocarbons such as toluene, xylene, ethylbenzene, etc., dialkyl ketones such as methyl
 5 ethyl ketone, etc. These may be used each alone or in combination of two or more. Moreover, other solvents such as aliphatic hydrocarbons, etc. can be mixed with the aromatic hydrocarbons in such a range as not reducing the solubility of polymerization products.
 10 These solvents are used preferably in the range of not exceeding 25% by weight based on the monomers. If amount of the solvent exceeds 25% by weight, polymerization rate conspicuously decreases and impact strength of the resulting resins greatly decreases.
 15 Furthermore, a large energy is required for recovery of the solvents to cause deterioration of economical efficiency. The solvent may be added after the polymerization has proceeded and viscosity has become relatively high, or it may be added before
 20 polymerization. When the solvent is added in a proportion of 5-20% by weight before polymerization, the quality becomes uniform, and this is preferred from the point of control of polymerization temperature.

Examples of general stabilizers are hindered
 25 phenol type antioxidants such as octadecyl-3-(3,5-tertiary-butyl-4-hydroxyphenyl) propionate, 4,6-bis(octylthiomethyl)-o-cresol, etc., phosphorus-based processing heat stabilizers such as tris(2,4-di-

tertiary-butylphenyl) phosphite, etc., and the like. These stabilizers may be used each alone or in combination of two or more. The time of addition is not particularly limited, and they may be added at
 5 either polymerization step or devolatilization step. Moreover, the stabilizers can be mixed with the product by a mechanical apparatus such as an extruder, Banbury mixer, or the like.

The apparatuses used in the polymerization
 10 step have no limitation and may be optionally selected in accordance with the polymerization method of the aromatic monovinyl monomers. For example, in the case of bulk polymerization, a polymerization apparatus comprising a first reactor, a second reactor and a
 15 third reactor can be used, and in the case of anionic polymerization, a polymerization apparatus such as an autoclave or the like can be used.

In the present invention, the devolatilization step has also no special limitation.
 20 In the case of carrying out the polymerization of aromatic monovinyl monomer by bulk polymerization, the polymerization is allowed to proceed until amount of unreacted aromatic monovinyl monomer finally reaches preferably not more than 50% by weight, more preferably
 25 not more than 40% by weight, and then devolatilization treatment is carried out by known method to remove volatile matters such as the aromatic monovinyl monomer and the like.

This devolatilization step is for removing unreacted materials and/or solvents from the reaction product after polymerization reaction, and for the devolatilization treatment, there can be used ordinary devolatilizing apparatuses such as flash drum, two-shaft devolatilizing machine, thin film evaporator, extruder, etc. Temperature for the devolatilization treatment is usually about 190-280°C. Pressure for the devolatilization treatment is usually 1-100 torr, preferably 1-50 torr, more preferably 1-10 torr. As devolatilizing method, preferred is to carry out the removal, for example, by reducing the pressure under heating or by passing through an extruder or the like designed for the purpose of removing volatile matters.

In the present invention, it is preferred that a 3-arylbenzofuranone represented by the above formula (I) (heat deterioration inhibitor) is added at the polymerization step or the devolatilization step. That is, in this case, the 3-arylbenzofuranone is added to a reactor used for the polymerization reaction or an extruder.

More preferably, 3-arylbenzofuranone is added after completion (preferably just after completion) of the polymerization step and before the devolatilization step, and in this case the 3-arylbenzofuranone is added at the outlet of the reactor used for the polymerization reaction.

For inhibition of heat decomposition of the

polymer, 3-arylbenzofuranone may further be added to the resulting product using a mechanical apparatus such as an extruder, a Banbury mixer or the like.

After 3-arylbenzofuranone (heat deterioration inhibitor) is added to a polymerization solution obtained at the polymerization step, it is preferred to mix them uniformly. This is because if 3-arylbenzofuranone is added to a reactor of inferior mixability or a polymerization line provided with no mixing means, dispersion of 3-arylbenzofuranone which is a heat deterioration inhibitor is insufficient, and although there is an effect to inhibit production of aromatic monovinyl monomer and dimers or trimers thereof at the devolatilization step, the effect is lowered and this is not preferred.

In order to uniformly mix the polymerization solution obtained at the polymerization step with 3-arylbenzofuranone (heat deterioration inhibitor), preferably, for example, a mixing apparatus is provided in addition to the polymerization apparatus and the devolatilization apparatus. The construction of the mixing apparatus has no special limitation, and any mixing apparatuses can be used as far as the polymerization solution obtained at the polymerization step can be uniformly mixed with 3-arylbenzofuranone. For example, there may be used complete mixing type mixers, column type mixers, etc. Specifically, the mixing apparatus can be provided behind the

polymerization apparatus (e.g., the third reactor).

In the method of the present invention, in case 3-arylbenzofuranone is added at the polymerization step, it is desirable to add the 3-arylbenzofuranone represented by the above formula (I) at the time when polymerization rate of the aromatic monovinyl monomer reaches not less than 50%, especially not less than 60%. The polymerization rate here means a ratio (%) of the weight of the polymerized polymer when weight of the starting monomer is assumed to be 100. If it is added at the beginning of polymerization, radicals at the polymerization reaction are trapped and this is not so preferred.

Furthermore, in case 3-arylbenzofuranone is added at the polymerization step, it is preferred to add it when the polymerization temperature at the polymerization step is not higher than 160°C. If the heat deterioration inhibitor is added after the polymerization temperature exceeds 160°C, radicals at the polymerization reaction are rapidly trapped and this is not so preferred.

When the polymerization is carried out by bulk-suspension polymerization, a partially polymerized product is dispersed in an aqueous medium with stirring using a suspension stabilizer such as calcium tertiary phosphate, polyvinyl alcohol or the like or using the suspension stabilizer in combination with a surface active agent, and the reaction is completed by

suspension polymerization. The resulting slurry containing suspension polymer particles is dehydrated, washed and then dried. Thereafter, unreacted materials in the dried suspension polymer particles are devolatilized, for example, by an extruder at the devolatilization step, and the polymer particles are pelletized. In this case, 3-arylbenzofuranone represented by the formula (I) is preferably added before the devolatilization step.

Furthermore, when anionic polymerization is carried out, the monomer is dissolved in an inert solvent, and polymerization is carried out using as a polymerization initiator an organic alkyl metal compound such as n-butyl lithium, sec-butyl lithium, t-butyl lithium, or the like. After termination of the polymerization, active terminals of the polymer are deactivated with a compound containing active hydrogen, such as methanol or the like to complete the polymerization. Thereafter, at the devolatilization step, unreacted materials and/or solvents are devolatilized from the reaction product after the polymerization reaction, for example, by a flash drum, a two-shaft devolatilizing machine, a thin film evaporator, an extruder, etc. and the product is pelletized. In this case, the 3-arylbenzofuranone represented by the formula (I) is added preferably before the devolatilization step.

Examples

The present invention will be explained in detail by the following examples and comparative examples, which should not be construed as limiting the invention in any manner.

[Preparation Example 1]

Preparation of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one

A mixture of 212.5 g (1.00 mole) of 2,4-di-tert-butylphenol (97%), 163.0 g (1.10 mole) of 50% aqueous glyoxylic acid and 0.5 g (2.6 millimoles) of p-toluenesulfonic acid monohydrate was added to 300 ml of 1,2-dichloroethane, followed by refluxing for 3.5 hours on a water separator in nitrogen. The resulting reaction mixture was concentrated, and the residue was taken in 800 ml of hexane and washed with water three times. The aqueous layer was further extracted with 300 ml of hexane, and the extract was combined with the organic layer, followed by drying with magnesium sulfate and then concentrating to obtain 260 g of a viscous compound.

500 ml of o-xylene was added to the resulting compound and 40 g of Fulcat 22B (trademark for sheet-like silicate manufactured by Laporte Adsorbents Co., Ltd.) was added thereto, followed by refluxing for 1.5 hours on a water separator. Then, Fulcat 22B was removed by filtration and excess o-xylene was distilled

off. The residue was crystallized from 400 ml of methanol to obtain 175.5 g of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one.

5 [Preparation Example 2]

Preparation of 5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-benzofuran-2-one

A mixture of 212.5 g (1.00 mole) of 2,4-di-tert-butylphenol (97%), 163.0 g (1.10 mole) of 50% aqueous glyoxylic acid and 0.5 g (2.6 millimoles) of p-toluenesulfonic acid monohydrate was added to 300 ml of 1,2-dichloroethane, followed by refluxing for 3.5 hours on a water separator in nitrogen. The resulting reaction mixture was concentrated, and the residue was taken in 800 ml of hexane and washed with water three times. The aqueous layer was further extracted with 300 ml of hexane, and the extract was combined with the organic layer, followed by drying with magnesium sulfate and then concentrating to obtain 262 g of a viscous compound.

500 ml of m-xylene was added to the resulting compound and 40 g of Fulcat 22B (trademark for sheet-like silicate manufactured by Laporte Adsorbents Co., Ltd.) was added thereto, followed by refluxing for 1.5 hours on a water separator. Then, Fulcat 22B was removed by filtration and excess m-xylene was distilled off. The residue was crystallized from 400 ml of methanol to obtain 242 g of 5,7-di-tert-butyl-3-(2,4-

dimethylphenyl)-3H-benzofuran-2-one.

Methods for analysis of the resin compositions and molded products in examples and
5 comparative examples are as follows.

(1) Measurement of weight average molecular weight:

Preparation of sample: About 1000 ppm of the resin composition was dissolved in tetrahydrofuran.

10 Conditions of measurement:

Device: Shodex 21 manufactured by Showa Denko K.K. (gel permeation chromatography)

Column: Sample: KF-806L 2 columns

Reference: KF-800RL 2 columns

15 Temperature: 40°C

Carrier: THF 1 ml/min

Detector: RI, UV: 254 nm

Calibration curve: Monodisperse PS
manufactured by Toso Co., Ltd.

20 Data processing: Sic-480

(2) Measurement of melt flow rate:

This was measured in accordance with ISO R1133 (conditions: 200°C, load 5 kgf).

(3) Measurement of residual amount of styrene
25 monomer in molded product:

Preparation of sample: 1 g of the resin composition was dissolved in 25 ml of dimethylformamide. Only when the polymer was

syndiotactic, 0.1 g of the resin composition was dissolved in dichlorobenzene.

Conditions of measurement:

Method of detection: FID

5 Device: GC14B manufactured by Shimadzu Construction Co., Ltd.

Column: CHROMAPACK CP WAX 52CB

100 m, film thickness 2 μm , 0.52 mm ϕ

Column temperature: 110°C - 10 min \rightarrow 15°C/min
10 \rightarrow 130°C - 2 min

Inlet temperature: 150°C

Detector temperature: 150°C

Carrier gas: Helium

(4) Measurement of the amount of 3-
15 arylbenzofuranone in molded product:

Preparation of sample: 1 g of the molded product was dissolved in methyl ethyl ketone.

Conditions of measurement:

Method of detection: FID

20 Device: GC17Apf manufactured by Shimadzu Construction Co., Ltd.

Column: DB-1 (100% dimethylpolysiloxane)

30 m, film thickness 0.1 μm , 0.25 mm ϕ

Column temperature: 100°C - 2 min \rightarrow 5°C/min \rightarrow
25 260°C - 5 min

Inlet temperature: 200°C

Detector temperature: 200°C

Carrier gas: Nitrogen

strip-shaped mold of 150 × 50 × 2.5 mm, short shots were conducted at a filling of 3.0 seconds. After termination of 70 shots, the injection molding was suspended for 15 minutes and the mold was cooled, and

5 the surface of the mold corresponding to the tip portion of the molded product was observed to examine the state of deposition of oil. Thereafter, while the state of deposition of oil onto the mold was similarly examined every 70 shots, the molding was repeated until

10 980 shots, and the number of shots when oil began to deposit onto the mold was obtained.

[Example 1]

0.05 Part by weight of a polymerization

15 initiator (1,1-bis(t-butylperoxy)-3,3,5-trimethylcyclohexane) was dissolved in 90 parts by weight of styrene and 10 parts by weight of ethylbenzene, and the solution was fed continuously and successively to a polymerization apparatus consisting

20 of a first reactor, a second reactor and a third reactor having a capacity of 1 liter each at a rate of 0.5 liter/hour. Just after termination of the above polymerization step, namely, at an outlet of the third reactor, 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-

25 benzofuran-2-one dissolved in ethylbenzene was added to the polymer obtained in the third reactor (weight average molecular weight = 260,000) in an amount of 0.15% by weight based on the polymer. Then, the

polymer and 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-
3H-benzofuran-2-one were uniformly mixed by a complete
mixing type mixer (capacity: 150 ml) provided behind
the third reactor, and the mixture was transferred to a
5 devolatilization apparatus consisting of two single-
screw extruders connected in series, and at this
devolatilization step volatile matters were
successively removed and the mixture was pelletized.

The conditions of polymerization reaction at
10 the polymerization step were as follows: The
polymerization temperature was 105-110°C and the number
of revolution of stirrer was 150 rpm in the first
reactor; the polymerization temperature was 115-125°C
and the number of revolution of stirrer was 50 rpm in
15 the second reactor; and the polymerization temperature
was 130-150°C and the number of revolution of stirrer
was 20 rpm in the third reactor. The polymerization
rates at the outlets of the respective reactors were
35% at the outlet of the first reactor, 65% at the
20 outlet of the second reactor, and 90% at the outlet of
the third reactor. At the devolatilization step, the
former single-screw extruder had a temperature of 190-
200°C and a degree of vacuum of 30 torr, and the latter
single-screw extruder had a temperature of 220-240°C and
25 a degree of vacuum of 5 torr.

Injection molded products for judgement on
odor were produced using the resulting pellets under
the following two different conditions. The first

condition is as follows: A molded product was obtained by usual continuous molding (product obtained without retention step). Another condition is as follows: Molding was once stopped and the resin was retained for 5 30 minutes in the cylinder, and then the molding was resumed, the resin obtained by the first two shots was abandoned, and the retained resin of the third shot was taken as a molded product (product obtained with a retention step of 30 minutes). Molding temperatures of 10 the respective zones of the injection molding machine were 250°C, 250°C, 230°C, and 210°C. Furthermore, the state of deposition of oil onto the mold at the time of injection molding was examined.

Residual amount of the styrene monomer, total 15 residual amount of the dimer and the trimer of the styrene monomer, results of judgement on the odor, color tone of the molded product by visual judgement, and state of deposition of oil onto the mold are shown in Table 1.

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[Example 2]

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H- 25 benzofuran-2-one was 0.05% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Example 3]

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.02% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Example 4]

Pellets and a molded product were produced in the same manner as in Example 1, except that 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was added at the position between the former extruder and the latter extruder of the single-screw extruder at the devolatilization step and the amount was 0.05% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Example 5]

Pellets and a molded product were produced in the same manner as in Example 1, except that 5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-benzofuran-2-one obtained in Preparation Example 2 was added in place of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one and the amount was 0.05% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Example 6]

Pellets and a molded product were produced in the same manner as in Example 1, except that 85 parts by weight of styrene and 5 parts by weight of polybutadiene (Diene 35 manufactured by Asahi Kasei K.K.) were used in place of 90 parts by weight of styrene, and they were evaluated on physical properties, etc. The results are shown in Table 1.

10 [Example 7]

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.02% by weight in Example 6, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Example 8]

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.01% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

25

[Example 9]

60 Kilograms of dehydrated cyclohexane and 10 kg of dehydrated styrene were charged in an autoclave

controlling the internal temperature to 80°C and the number of revolution to 200 rpm. Continuous polymerization was carried out for 5 hours with feeding to this reactor styrene at a rate of 1 liter/hour, and, besides, methylaminoxane at a rate of 75 millimoles/hour and pentamethylcyclopentadienyltitanium trimethoxide at a rate of 0.15 millimole/hour as catalysts. Powders discharged from the outlet of the reactor were immersed in methanol in which 1% by weight of sodium hydroxide was dissolved, and were washed. Thereafter, to the resulting polymer was added 0.01% by weight of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one at the inlet of the 20 mm single-screw extruder, followed by drying at 180°C under 10 torr for 1 hour by a dryer. The polymer before adding the additives thereto was 97% in syndiotacticity at racemic pentad by ¹³C-NMR.

The polymer was subjected to devolatilization and pelletization by the above single-screw extruder at an extruder temperature of 270-290°C and a degree of vacuum of 20 torr.

Injection molded products for judgement on odor were produced using the resulting pellets under two different conditions. The first condition is as follows: A molded product was obtained by usual continuous molding (without retention step). Another condition is as follows: Molding was once stopped and the resin was retained for 30 minutes in the cylinder,

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.005% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Comparative Example 3]

Pellets and a molded product were produced in the same manner as in Example 1, except that SUMILIZER GS (a trademark for phenolic heat deterioration inhibitor manufactured by Sumitomo Chemical Co., Ltd.; chemical name: 2-[1-(2-hydroxy -3,5-di-tert-pentylphenyl)ethyl]-4,6-di-tert-pentylphenyl acrylate) was used in place of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one, and the amount was 0.05% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Comparative Example 4]

Pellets and a molded product were produced in the same manner as in Example 1, except that SUMILIZER GS (a trademark for phenolic heat deterioration inhibitor manufactured by Sumitomo Chemical Co., Ltd.) was used in place of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one, and the amount was 0.3% by weight, and they were evaluated on physical properties, etc. The results are shown in Table 1.

[Comparative Example 5]

Pellets and a molded product were produced in the same manner as in Example 1, except that the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.005% by weight and 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was

Table 1

	Deterioration inhibitor		Pellet discharged from polymerization apparatus		Injection molded product (No retention)		Injection molded product (Retention for 30 minutes)			The number of shots before deposition of oil
	Kind *1	Amount (wt%)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components *2 (wt%)	Visual judgement on color tone *3	Judgement on odor *4	Residual amount of styrene monomer (ppm)	Visual judgement on color tone *3	Judgement on odor *4	
Example 1	ABF1	0.15	43	0.11	O	O	44	O	O	700
Example 2	ABF1	0.05	57	0.14	O	O	59	O	O	630
Example 3	ABF1	0.02	68	0.21	O	O	74	O	O	560
Example 4	ABF1	0.05	59	0.17	O	O	61	O	O	630
Example 5	ABF2	0.05	59	0.15	O	O	61	O	O	630
Example 6	ABF1	0.15	40	0.09	O	O	41	O	O	700
Example 7	ABF1	0.02	64	0.18	O	O	69	O	O	630
Example 8	ABF1	0.01	80	0.32	O	O	95	O	O	490
Example 9	ABF1	0.01	85	0.04	O	O	90	O	O	910
Example 10	ABF1	0.01	30	0.01>	O	O	85	O	O	980
Comparative Example 1	-	-	165	0.50	x	x	215	xx	x	210
Comparative Example 2	ABF1	0.005	140	0.45	x	x	160	x	x	280
Comparative Example 3	GS	0.05	122	0.29	x	x	140	x	x	490
Comparative Example 4	GS	0.3	55	0.16	xx	O	70	xx	O	560
Comparative Example 5	ABF1	0.005	87	0.44	O	O	110	x	x	280
Comparative Example 6	ABF1	0.05	130	0.15	x	x	135	x	x	630
Comparative Example 7	ABF1	0.01	120	0.04	x	x	127	x	x	910
Comparative Example 8	ABF1	0.01	118	0.01>	x	x	152	x	x	980

*1 ABF1=5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one, ABF2=5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-benzofuran-2-one, GS=SUMILIZER GS

*2: Low molecular components = Total of dimer and trimer of styrene monomer

*3: Visual judgement on color tone; O Colorless, x Somewhat yellow, xx Yellow

*4: Judgement on odor; O No odor, x Odor development

It can be seen from Table 1 that molded products highly excellent in color tone can be obtained by adding 3-arylbenzofuranone represented by the formula (I) in a given amount and setting the residual amount of the styrene monomer at not more than 100 ppm. If the residual amount of the styrene monomer is larger, color tone of the resulting molded products is considerably deteriorated even when the heat deterioration inhibitor is added in the given amount. Furthermore, when they are subjected to residence test in molding machines, the resin compositions of the present invention are less in increase of the amounts of the styrene monomer and dimer or trimer thereof, and the products do not change in color tone and are very excellent in heat stability. Moreover, the resin compositions of the present invention contain the dimer and trimer in an amount of not more than 0.4% by weight in total, cause less deposition of oil to the mold, and are much superior in moldability.

Further, when the phenolic heat deterioration inhibitor (SUMILIZER GS) is used, the resulting products are considerably bad in color tone. It can be further seen that even when amount of the phenolic heat deterioration inhibitor is the same as that of 3-arylbenzofuranone of the present invention, the effect to diminish the styrene monomer and the dimer or the trimer is lower than 3-arylbenzofuranone of the present invention.

Evaluations (i) of foamed sheets produced using the resin composition of the present invention and formed products made from the sheets were conducted.

5 Methods of evaluation on the resins used in the following Examples 11-19 and Comparative Examples 9-11 are as follows.

(1) Method of evaluation of the foamed sheets on formability:

10 For determination of formability of the foamed sheets, it was examined whether formed products could be obtained from the foamed sheets by a small forming machine with changing the oven temperature to 200°C, 220°C and 240°C for a constant heating time.

15 (2) Method of measurement of unevenness in thickness of the formed products:

In ten samples of formed products shown in FIG. 1 obtained from the foamed sheets, thickness of four positions (A, B, C, D) of the same side face was
20 measured, and standard deviation thereof was obtained and this was taken as an indication of unevenness in thickness.

(3) Method of judgement on appearance of the formed products and transferability in printing:

25 Surface roughness of the formed products was visually examined. The transferability in printing was judged by visual examination of the transferability of letters printed.

[Examples 11-19 and Comparative Examples 9-10]

The resins used for producing the foamed sheets were those which were produced in Examples 1-9 and Comparative Examples 1-2 and mentioned in the column "Resins used for evaluation of foamed sheets" in Table 2.

[Comparative Example 11]

A resin was produced in the same manner as in Example 2, except that the polymerization initiator (1,1-bis(t-butylperoxy)-3,3,5-trimethylcyclohexane) was not added, and the polymerization temperature in the first reactor was 125-130°C, that in the second reactor was 135-145°C and that in the third reactor was 150-165°C (polymerization rate at the outlet of the third reactor: 90%).

<Method for producing a formed product using a foamed sheet of the aromatic monovinyl resin composition>

Using a 30 mm extrusion foaming machine provided with a T-die of 30 mm in width, a foamed sheet of about 8 times was obtained from 100 parts by weight of the aromatic monovinyl resin composition to which 1 part by weight of a foaming nucleator and 3 parts by weight of a foaming agent were added. Temperature of resin melting zone was adjusted to 180-230°C, that of rotary cooler was adjusted to 150-160°C and that of T-die was adjusted to 120-130°C. The foaming nucleator

used was MISTRON VAPOR manufactured by Japan Mistron Co., Ltd. and the foaming agent used was a mixture of 65% by weight of n-butane and 35% by weight of i-butane.

5 The resulting foamed sheet was cured for 1 week and heated for 15 seconds at a given oven temperature, and then a box-shaped formed product of 100 mm square, 50 mm deep and about 2-3 mm thick was produced by a mold adjusted to 60°C using a small
10 forming machine. For determination of forming width at the forming, it was tested whether production of a formed product was possible or not at the three points of oven temperature of 200°C, 220°C and 240°C. Furthermore, measurement of unevenness in thickness and
15 visual examination of appearance of the formed product obtained at the oven temperature of 200°C were conducted.

Residual amount of the styrene monomer, total residual amount of the dimer and the trimer of the
20 styrene monomer, formability of the foamed sheet, unevenness in thickness of the formed product, results of visual examination of appearance are shown in Table 2.

Table 2

	Resin used for evaluation of foamed sheet	Deteriora- tion inhibitor	Pellet discharged from polymerization apparatus			Foamed sheet					Formed product		
			Kind Amount *1 (wt%)	Residual amount of styrene monomer (ppm)	Residual amount of low mole- cular components *2 (wt%)	Melt flow (g/10 min)	Residual amount of styrene monomer (ppm)	Residual amount of low mole- cular component s *2 (wt%)	Formability			Standard deviation of uneven- ness in thickness (mm) *3	Appear- ance *4
									Forming possible: O Impossible: x				
									Heating time (15 sec) Heating temperature (°C)				
			200	220	240								
Example 11	Example 1	ABF1 0.15	43	0.11	1.5	42	0.11	O	O	O	O	0.1	O
Example 12	Example 2	ABF1 0.05	57	0.14	1.7	57	0.13	O	O	O	O	0.1	O
Example 13	Example 3	ABF1 0.02	68	0.21	1.7	70	0.22	O	O	O	O	0.1	O
Example 14	Example 4	ABF1 0.05	59	0.17	1.7	58	0.16	O	O	O	O	0.1	O
Example 15	Example 5	ABF2 0.05	59	0.15	1.7	59	0.15	O	O	O	O	0.1	O
Example 16	Example 6	ABF1 0.15	40	0.09	1.5	41	0.09	O	O	O	O	0.15	O
Example 17	Example 7	ABF1 0.02	64	0.18	1.7	67	0.19	O	O	O	O	0.15	O
Example 18	Example 8	ABF1 0.01	80	0.32	1.8	89	0.35	O	O	O	O	0.15	O
Example 19	Example 9	ABF1 0.01	85	0.04	1.7	89	0.07	O	O	O	O	0.1	O
Compara- tive Example 9	Compara- tive Example 1	-	165	0.50	1.9	213	0.61	O	O	O	x	0.35	x
Compara- tive Example 10	Compara- tive Example 2	ABF1 0.005	140	0.45	1.8	162	0.53	O	O	O	x	0.3	x
Compara- tive Example 11	-	ABF1 0.05	65	0.80	1.8	66	0.81	O	x	x	x	0.5	x

*1: ABF1 = 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one

ABF2 = 5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-benzofuran-2-one

*2: Low molecular components = Total of dimer and trimer of styrene monomer

*3: Unevenness in thickness = Standard deviation of thickness of side face (2-3mm) of formed product

*4: Appearance (surface gloss and gloss unevenness) O : Good x : Bad

Evaluations (ii) of foamed sheets produced using the resin composition of the present invention and formed products produced from the sheets were conducted.

5

[Example 20]

A resin composition was produced under nearly the same production conditions as in Example 1, except that the reaction apparatus used was 10 times in size, and the amount of 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one was 0.05% by weight. Using the resulting pellets, a foamed sheet and a formed product were produced by the following method.

15 <Method for producing a formed product using
a foamed sheet of the aromatic monovinyl resin
composition>

To 100 parts by weight of the aromatic monovinyl resin composition were added 0.5 part by weight of talc as a foaming nucleator and 0.3 part by weight of zinc stearate as a dispersing aid, followed by well stirring and mixing them by mixer and then feeding the mixture to a hopper of a 65 mm single-screw extruder having an L/D of 33. Then, the mixture was melt kneaded at the former stage of the screw of the extruder at 235°C, and a mixture of 65% by weight of n-butane and 35% by weight of i-butane was poured from a foaming agent pouring hole provided at the intermediate

stage of the extruder so that the amount of the mixture was 2.5% by weight based on the total amount of extrudate.

Then, the kneaded product was cooled to 160°C at the latter stage of the screw of the extruder and subjected to foaming extrusion from a ring die in a tubular form. The resulting tubular foamed sheet was cooled in a mandrel of the extruder and then one face thereof was cut open by a cutter to obtain a foamed sheet. The foamed sheet for visual examination and for producing a formed product was taken after continuous operation of the extruder for 1 hour and was cured for 1 week. After visual examination, this foamed sheet was heated for 10 seconds in an oven of 200°C, and then a box-shaped formed product of 100 mm square and 40 mm deep was produced by a mold adjusted to 60°C using a small forming machine. After visual examination, letters were printed on the formed product and transferability was evaluated.

Residual amount of the styrene monomer, total residual amount of the dimer and the trimer of the styrene monomer, appearance of the foamed sheet, appearance of the formed product and printability are shown in Table 3.

[Example 21]

A resin composition and a formed product were produced in the same manner as in Example 20, except

that the degree of vacuum in the latter stage of the single-screw extruder at the devolatilization step was 10 torr, and they were evaluated on physical properties, etc. The results are shown in Table 3.

5

[Comparative Example 12]

A resin composition and a formed product were produced in the same manner as in Example 20, except that the degree of vacuum in the latter stage of the single-screw extruder at the devolatilization step was 40 torr, and they were evaluated on physical properties, etc. The results are shown in Table 3.

Table 3

	Deterioration inhibitor		Pellet discharged from polymerization apparatus			Foamed sheet		Formed product	
	Kind *1	Amount (wt%)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components *2 (wt%)	Melt flow rate (g/10 min)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components *2 (wt%)	Appearance *3	Transferability in printing *4
Example 20	ABF1	0.05	58	0.14	1.8	63	0.16	O	O
Example 21	ABF1	0.05	80	0.14	1.7	87	0.17	O	O
Comparative Example 12	ABF1	0.05	400	0.16	1.7	412	0.18	X	X

*1 ABF1=5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one

*2: Low molecular components = Total of dimer and trimer of styrene monomer

*3: Appearance (surface gloss and gloss unevenness) O: Good x: Bad

*4: Transferability in printing

Degree of Transferability of letters 0: Good x : Bad

[illegible]

It can be seen from Table 2 and Table 3 that when the residual amount of the styrene monomer is not more than 100 ppm and the total residual amount of the dimer and the trimer of the styrene monomer is not more than 0.4% by weight, foamed sheets excellent in formability can be obtained and formed products less in unevenness of thickness and very excellent in appearance and printability can be obtained. Furthermore, the resin composition of the present invention is very excellent in heat stability in production of foamed sheets.

Moreover, non-foamed sheets produced using the resin composition of the present invention and formed products made from the non-foamed sheets were evaluated.

Methods for evaluation of the resins used in the following Examples 22-30 and Comparative Examples 13-17 are as follows.

(1) Methods for judgement on die lines and foreign matters at the dice part:

Presence of die lines was visually examined by observing the surface of the resin sheet with a magnifying lens of five magnifications. The foreign matters at dice part was visually examined.

(2) Method for judgement on appearance:

Foreign matters and irregularity of the surface were visually examined with a magnifying lens of five magnifications.

[Examples 22-30 and Comparative Examples 13-17]

The resins used for producing the resin sheets were those which were produced in Examples 1-9 and Comparative Examples 1, 2, 5, 12 and 11 and mentioned in the column "Resins used for evaluation of resin sheets" in Table 4. Methods for producing the resin sheet and the formed product are shown below.

<Method for producing a formed product using a sheet of the aromatic monovinyl resin composition>

Using a 30 mm extruder provided with a T-die of 40 mm in width, a sheet of 300 mm in width and 1 mm in thickness was taken off by rolls, and continuous operation was carried out for 3 hours. Then, ten sheets of 300 mm in length were collected, and, simultaneously, presence or absence of deposition of foreign matters at the resin outlet of T-die was examined. Temperature of resin melting zone was adjusted to 200-250°C, and that of T-die was adjusted to 220-240°C. The collected sheets were heated to 130-140°C, and then box-shaped formed products of 100 mm square and 50 mm deep were produced by vacuum forming using a small pressure forming machine.

Residual amount of the styrene monomer, total residual amount of the dimer and the trimer of the styrene monomer, die lines of the resin sheets, presence or absence of foreign matters at the dice part, and appearance of the formed product are shown in Table 4.

Table 4

	Resin used for evaluation of foamed sheet	Deterioration inhibitor		Pellet discharged from polymerization apparatus			Resin sheet				Foreign matters at dice *3	Appearance of molded product *4
		Kind *1	Amount (wt%)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components *2 (wt%)	Melt flow (g/10 min)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components *2 (wt%)	Die lines *3			
Example 22	Example 1	ABF1	0.15	43	0.11	1.5	42	0.11	0	0	0	
Example 23	Example 2	ABF1	0.05	57	0.14	1.7	57	0.13	0	0	0	
Example 24	Example 3	ABF1	0.02	68	0.21	1.7	70	0.22	0	0	0	
Example 25	Example 4	ABF1	0.05	59	0.17	1.7	58	0.16	0	0	0	
Example 26	Example 5	ABF2	0.05	59	0.15	1.7	58	0.15	0	0	0	
Example 27	Example 6	ABF1	0.15	40	0.09	1.5	41	0.09	0	0	0	
Example 28	Example 7	ABF1	0.02	64	0.18	1.7	67	0.19	0	0	0	
Example 29	Example 8	ABF1	0.01	80	0.32	1.8	89	0.35	0	0	0	
Example 30	Example 9	ABF1	0.01	85	0.04	1.7	89	0.07	0	0	0	
Comparative Example 13	Comparative Example 1	-	-	165	0.50	1.9	213	0.61	x	x	x	
Comparative Example 14	Comparative Example 2	ABF1	0.005	140	0.45	1.8	162	0.53	x	x	x	
Comparative Example 15	Comparative Example 5	ABF1	0.005	87	0.44	1.8	120	0.52	x	x	x	
Comparative Example 16	Comparative Example 12	ABF1	0.05	400	0.16	1.7	511	0.15	x	0	x	
Comparative Example 17	Comparative Example 11	ABF1	0.05	65	0.80	1.8	65	0.81	0	x	x	

*1: ABF1 = 5,7-di-tert-butyl-3-(3,4-dimethylphenyl)-3H-benzofuran-2-one

ABF2 = 5,7-di-tert-butyl-3-(2,4-dimethylphenyl)-3H-benzofuran-2-one

*2: Low molecular components = Total of dimer and trimer of styrene monomer

*3: Die lines and foreign matters at dice part O: No x: Present

*4: Appearance (foreign matters, surface irregularities, etc.) O: Good x: Bad

Table 5

	Polymerization method	Heat deterioration inhibitor				Degree of vacuum of former/latter extruders (torr)	Pellet discharged from polymerization apparatus	
		Kind*1	Amount (wt%)	Position of addition	Mixing apparatus	Temperature of polymerization solution at the position of addition (°C)	Residual amount of styrene monomer (ppm)	Residual amount of low molecular components*3 (wt%)
Example 1	Continuous bulk polymerization	ABF1	0.15	Outlet of the third reactor	Used	150	43	0.11
Example 2	Continuous bulk polymerization	ABF1	0.05	Outlet of the third reactor	Used	150	57	0.14
Example 3	Continuous bulk polymerization	ABF1	0.02	Outlet of the third reactor	Used	150	68	0.21
Example 4	Continuous bulk polymerization	ABF1	0.05	Between extruders	Used	150	59	0.17
Example 5	Continuous bulk polymerization	ABF2	0.05	Outlet of the third reactor	Used	150	59	0.15
Example 6	Continuous bulk polymerization	ABF1	0.15	Outlet of the third reactor	Used	150	40	0.09
Example 7	Continuous bulk polymerization	ABF1	0.02	Outlet of the third reactor	Used	150	64	0.18
Example 8	Continuous bulk polymerization	ABF1	0.01	Outlet of the third reactor	Used	150	80	0.32
Example 9	Anionic polymerization	ABF1	0.01	Inlet of extruder	-	-	85	0.04
Example 10	Ionic-polymerization*2	ABF1	0.01	Inlet of extruder	-	-	30	0.01>
Example 31	Continuous bulk polymerization	ABF1	0.05	Outlet of the third reactor	Not used	150	65	0.19
Example 32	Continuous bulk polymerization	ABF1	0.05	The third reactor	Used	150	62	0.16
Example 33	Continuous bulk polymerization	ABF1	0.05	The third reactor	Used	160	85	0.28
Comparative Example 1	Continuous bulk polymerization	-	-	-	-	-	165	0.50
Comparative Example 2	Continuous bulk polymerization	ABF1	0.005	Outlet of the third reactor	Used	150	140	0.45
Comparative Example 18	Continuous bulk polymerization	ABF1	0.05	Inlet of the first reactor	Used	-	167	0.52

*1: ABF1 = 5, 7-di-tert-butyl-3-(3, 4-dimethylphenyl)-3H-benzofuran-2-one

ABF2 = 5, 7-di-tert-butyl-3-(2, 4-dimethylphenyl)-3H-benzofuran-2-one

*2: Ionic polymerization using metallocene catalyst

*3: Low molecular components = Total of dimer and trimer of styrene monomer

It can be seen from Table 5 that residual amount of styrene monomer and total residual amount of dimer and trimer of the styrene monomer can be markedly reduced by adding the specific amount of 3-arylbzofuranone of the present invention at the third reactor in the polymerization step, at the outlet of the third reactor which is just after the polymerization step (before devolatilization step) or at the position between the former single-screw extruder and the latter single-screw extruder in the devolatilization step. Furthermore, amounts of the above-mentioned low molecular weight components can be further reduced by uniformly mixing the polymerization solution obtained at the polymerization step with the heat deterioration inhibitor using a mixing equipment after the addition of the heat deterioration inhibitor. Moreover, in the case of adding the heat deterioration inhibitor at the polymerization step, amounts of the low molecular weight components can be further reduced by adding the heat deterioration inhibitor at the position of higher polymerization rate and low polymerization temperature.

Industrial Applicability

As mentioned above, the aromatic monovinyl resin composition of the present invention is excellent in moldability and heat stability at the molding and can be made into products satisfactory in color tone

and less in development of odor. In addition, the composition of the present invention can be suitably used as extruded sheets (foamed or non-foamed) and molded products made by injection molding, blow molding and the like, and there can be obtained particularly suitable products for packaging materials and containers which directly contact with foods, etc. Furthermore, the aromatic monovinyl resin composition of the present invention can be widely employed for uses such as toys, miscellaneous goods, daily necessities, electrical parts, various industrial parts, etc., and, thus, it plays an important part in the industrial world.